

1 What is claimed is:

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3 1. A method of removing  $\text{SO}_3$  from off gases produced at an industrial plant which combusts sulfur  
4 containing fuels, the method comprising the steps of:

5  
6 providing a sulfur containing fuel as a power source for the plant;

7  
8 burning the fuel at the plant, thereby producing off gases containing  $\text{SO}_3$ , and collecting the off gases  
9 in an exhaust duct which is heated by the off gases to an exhaust duct temperature;

10  
11 injecting a calcium hydroxide slurry of controlled and specified physical and chemical characteristics  
12 into the off gases in the exhaust duct at a point in the duct where the exhaust duct temperature is  
13 sufficient to evaporate water from the calcium hydroxide slurry, the calcium hydroxide reacting with  
14 the  $\text{SO}_3$  to produce calcium sulfate;

15  
16 removing the calcium sulfate in a particulate removal system.

17  
18 2. The method of claim 1, wherein the calcium hydroxide slurry is injected at a point in the duct  
19 where the exhaust duct temperature is below about 500-600EC.

20  
21 3. The method of claim 1, wherein the calcium hydroxide slurry is made by slaking quicklime.

22  
23 4. The method of claim 1, wherein the solids content of the calcium hydroxide slurry is in the range  
24 from about 15-45% by weight.

25  
26 5. The method of claim 1, wherein the calcium hydroxide slurry is made by adding additional water  
27 to lime hydrate.

1 6. The method of claim 1, where the industrial plant has a wet scrubbing system which utilizes wet  
2 slaking of calcium oxide for the removal of oxides of sulfur in off gases and wherein a portion of the  
3 wet slaked calcium oxide is diverted from the wet scrubbing system and injected into the exhaust gas  
4 duct prior to the particulate removal system.

5  
6 7. The method of claim 1, wherein a saturated solution of calcium hydroxide is injected into the  
7 exhaust duct.

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9 8. The method of claim 1, wherein the calcium hydroxide slurry is introduced into the exhaust duct  
10 through at least one nozzle and wherein compressed air is also introduced into the nozzle to produce  
11 a plurality of lime slurry droplets, the lime slurry droplets having a particle size in the range from  
12 about 30-100 microns.

13  
14 9. A method of removing  $\text{SO}_3$  from off gases produced at a fossil fired power plant having a boiler,  
15 an exhaust duct which receives off gases from a combustion chamber of the boiler and a downstream  
16 particulate removal station, the method comprising the steps of:

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18 providing a fossil fuel as a power source for the plant;

19  
20 burning the fossil fuel in the combustion chamber of the boiler at the plant, thereby producing off  
21 gases containing  $\text{SO}_3$ , and collecting the off gases in the exhaust duct which is heated by the off gases  
22 to an exhaust duct temperature;

23  
24 injecting a calcium hydroxide slurry of controlled and specified physical and chemical characteristics  
25 into the off gases downstream from the boiler but upstream from the particulate removal station, the  
26 calcium hydroxide slurry being injected in the exhaust duct at a point in the duct where the exhaust  
27 duct temperature is sufficient to evaporate water from the calcium hydroxide slurry but is low enough  
28 to avoid decomposing and converting the calcium hydroxide to calcium oxide, the calcium hydroxide  
29 reacting with the  $\text{SO}_3$  to produce calcium sulfate;

1 removing the calcium sulfate at the particulate removal station.

2  
3 10. The method of claim 9, wherein the exhaust gas duct passes to an electrostatic precipitator and  
4 from the electrostatic precipitator to a flue gas desulfurization absorber, and wherein the calcium  
5 hydroxide slurry is injected at a point in the exhaust duct between the electrostatic precipitator and  
6 the flue gas desulfurization absorber.

7  
8 11. The method of claim 10, wherein the calcium hydroxide slurry is injected at a point in the duct  
9 where the exhaust duct temperature is below about 500-600EC.

10  
11 12. The method of claim 10, wherein the calcium hydroxide slurry is made by slaking quicklime.

12  
13 13. The method of claim 10, wherein the solids content of the calcium hydroxide slurry is in the  
14 range from about 15-35% by weight.

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16 14. The method of claim 10, wherein the calcium hydroxide slurry is made by slaking quicklime on  
17 site at the plant using a portable slaking tank.

18  
19 15. The method of claim 10, where the power plant has a wet scrubbing system which utilizes wet  
20 slaking of calcium oxide for the removal of oxides of sulfur in off gases and wherein a portion of the  
21 wet slaked calcium oxide is diverted from the wet scrubbing system and injected into the exhaust gas  
22 duct prior to the particulate removal system.

23  
24 16. The method of claim 10, wherein a saturated solution of calcium hydroxide is injected into the  
25 exhaust duct.

26  
27 17. The method of claim 10, wherein the calcium hydroxide slurry is introduced into the exhaust duct  
28 through at least one nozzle and wherein compressed air is also introduced into the nozzle to produce

- 1 a plurality of lime slurry droplets, the lime slurry droplets having a particle size in the range from
- 2 about 40-50 microns.